

A MIXTURE MODEL FOR THE DYNAMIC OF THE GUT MUCUS LAYER

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Abstract. We introduce a mixture model intended to describe the dynamics of the mucus layer that wraps the gut mucosa. This model takes into account the fluid mechanics of the gut content, the inhomogeneous rheology that depends on the fluid composition, and the main physiological mechanisms that ensure the homoeostasis of the mucus layer. Numerical simulations, based on a finite volume approach, prove the ability of the model to produce a stable steady-state mucus layer. We also perform a sensitivity analysis by using a meta-model based on polynomial chaos in order to identify the main parameters impacting the shape of the mucus layer. The effect of the interaction of the mucus with a population of bacteria is eventually discussed.

Résumé. Nous présentons un modèle de mélange qui décrit l'évolution de la couche de mucus qui recouvre la muqueuse du gros intestin. Ce modèle prend en compte la mécanique des fluides qui composent le contenu intestinal, la rhéologie inhomogène dépendant de la composition du fluide et les principaux mécanismes physiologiques qui assurent l'homéostasie de la couche de mucus. Des résultats numériques, obtenus par une méthode volumes finis, démontrent la capacité du modèle à reproduire une couche de mucus stationnaire stable. Nous pratiquons ensuite une analyse de sensibilité en construisant un métamodèle basé sur des polynômes de chaos afin d'identifier les paramètres impactant le plus la forme de la couche de mucus. Finalement, nous discutons les effets des interactions entre la couche de mucus et une population bactérienne chimiotactique.

1. INTRODUCTION

The distal human gut, also known as colon, is inhabited by a complex microbial ecosystem, the gut microbiota. Recent progresses in the knowledge of the microbiota structure and function have demonstrated its direct or indirect implication in various affections, among which Crohn's disease, allergic and metabolic disorders, obesity, cholesterol or possibly autistic disorders. Understanding the gut microbiota ecology is one of the current scientific hot-spot in microbiology. The gut microbiota provides to his human host several benefits, such as energy harvesting [20], barrier function against pathogens and immune system maturation [21]. However, even these beneficial commensal bacteria represent an infection threat for the host. Alongside with complex active immune mechanisms, a first simple and passive protection is an insulating layer of mucus that physically separates the microbial populations from the host tissues.

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This mucus barrier is actually composed of two distinct layers with different rheological characteristics. A first viscous layer wraps the epithelial cells. An external, thicker and more fluid layer covers the first one [13]. These rheological discrepancies are attributed to structural differences in the mucus protein folding and to hydration/dehydration effects. The active water pumping of the intestinal mucosa dries out the inner layer of mucus, whereas the liquid luminal content keeps the outer layer hydrated. Mucus turn over results from the erosion of the external layer by the luminal flux and the continuous renewal of the inner layer by the mucosa [23]. Unlike the inner layer, the outer layer can be penetrated by bacteria, which thereby take advantage of this food source, resist the luminal flow and increase their residence time in the gut. It represents an ecological niche that influences the global equilibrium of the gut microbiota. A good model of its dynamics is then a key issue in the perspective of constructing accurate models of the gut microbiota ecology. This modelling work could help physiologists and microbiologists to better describe and understand the main parameters in mucus layer formation or disruption and to study host-microbiota interactions and microbiota ecology in an integrative way.

Since there is no sharp interface between the mucus and the luminal liquid, our approach adopts the mixture flows framework. Further details about the mixture theory can be found in [19, 24]. It leads to systems of Partial Differential Equations (PDE) describing a mixture of several components with different physical properties. For adaptation of mixture theory for describing biological flows, we refer the reader to [14] (poro-elastic materials), [18] (tumor growth), and [6] (growth of phototrophic biofilms). The formation of layers of biological mucus can also be described at the molecular scale [11]. A compartmental model, written in terms of a large set of Ordinary Differential Equations describing fibre degradation by gut microbial populations, has been proposed in [16]. In this 0D model, the mucus is modelled as a separate compartment but spatial mechanisms are loosely described and the underlying fluid mechanics is discarded. A model based on the principles of fluid mechanics for pulmonary mucus appeared in [5]; it describes mucus evacuation by cilia without investigating the dynamics of the mucus layer formation. To our knowledge, the present work is the first attempt of a fluid mechanics model specially designed to describe the intestinal fluid flows involved in the constitution of the ecological environment of the gut microbiota. Together with adapted population dynamics and host response models, it constitutes a key component of a global ecological model of intestinal microbial communities.

We organize the article as follows. We introduce the mixture model of intestinal fluid flow in Section 2. Section 3 focuses on the boundary conditions and sketches the derivation of an approximate model. Section 4 details the numerical method used for the simulation of the model and test cases are presented in Section 5. We analyse the sensitivity of the approximate model in Section 6. Finally, we extend the model by including a chemotactic bacterial population in the mixture model in Section 7.

2. A MIXTURE MODEL FOR THE FLUID DYNAMICS IN THE HUMAN GUT

2.1. Mathematical modelling of the gut content

A schematic view of the gut, which makes the length scales precise, is represented on Fig. 1a; the mucus layer (in green) measures about four millimeters. In what follows, the geometry is drastically simplified and curvature effects are neglected: we will simply work on a 2D rectangular domain Ω_D , delimited by two lateral boundaries $\Gamma_l(x = -L_x), \Gamma_r(x = L_x)$, that represent the gut mucosa, the superior boundary $\Gamma_{in}(y = 0)$ and the inferior boundary $\Gamma_{out}(y = -L_y)$ which stand respectively for the inflow and outflow boundaries.

We assume in this model that the gut content is a mixture of two components: the mucus and the luminal content. Let $M(t, X)$ and $L(t, X)$ be the volume fractions, at time $t > 0$ and position $X = (x, y) \in \Omega_D$, occupied by the mucus and the liquid luminal phase, respectively. We then have, for all t and X

$$M(t, X) + L(t, X) = 1. \quad (1)$$

Both components of the mixture are supposed to be transported by a common velocity field, hereafter denoted by $V(t, X) = (u, v)(t, X)$. It represents the bulk velocity of the mixture. The mixture model incorporates interface effects through diffusive terms in the continuity equations for M and L . Let us denote by D_M (resp.

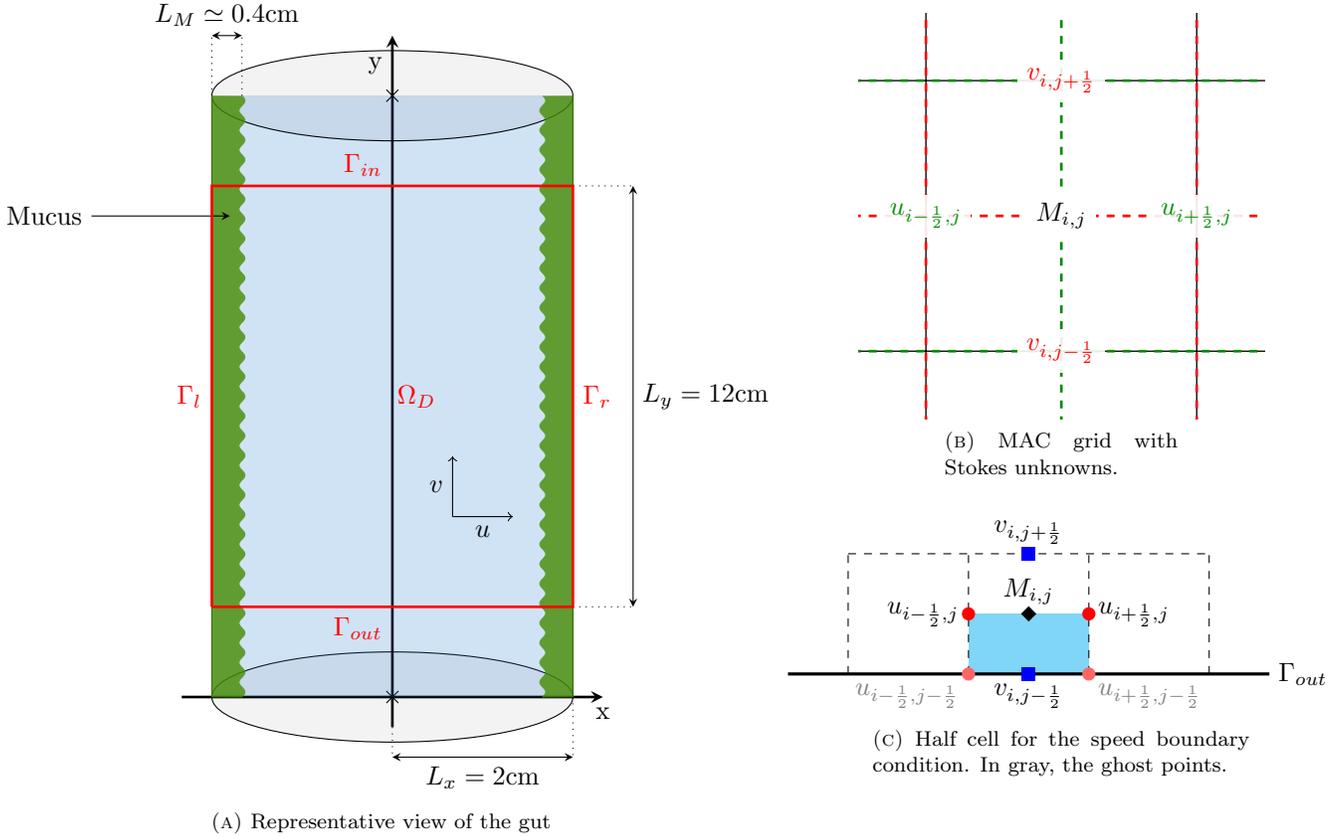


FIGURE 1. Computation domain and illustration of the MAC discretization — See Section 4.

D_L) the diffusion coefficient for M (resp. L). The mass conservation equations then read

$$\partial_t M + \nabla_X \cdot (MV - D_M \nabla_X M) = 0, \quad (2)$$

$$\partial_t L + \nabla_X \cdot (LV - D_L \nabla_X L) = 0. \quad (3)$$

The velocity field $(t, X) \mapsto V(t, X)$ is determined using fluid mechanics principles. Since the Reynolds number is low, we neglect convective effects and we use the Stokes equations. The velocity is solution of

$$-\nabla_X \cdot (\mu(M) (\nabla_X V + \nabla_X V^T)) + \nabla_X P = 0 \quad (4)$$

where $\mu(M)$ is the viscosity and P is the hydrostatic pressure. The viscosity is a function of the mucus volume fraction, bearing in mind that μ is much larger in the mucus than in the fluid. Summing Eq. (2) and (3), and using Eq. (1), we are led to the following constraint

$$\nabla_X \cdot V = \nabla_X \cdot ((D_M - D_L) \nabla_X M). \quad (5)$$

In order to detail the modeling assumption, it is convenient to introduce the velocity fields

$$u_M(t, X) = V - D_M \nabla_X \ln(M), \quad u_L(t, X) = V - D_L \nabla_X \ln(L). \quad (6)$$

Then the continuity equations can be rewritten in the more conventional form

$$\partial_t M + \nabla_X \cdot (Mu_M) = 0 = \partial_t L + \nabla_X \cdot (Lu_L)$$

by means of the constituents' velocities u_M and u_L . The constraint (5) traduces the fact that the mean volume velocity $Mu_M + Lu_L$ is solenoidal. Eq. (6) is a constitutive law, it has the form of a Fick's law for the relative velocities $u_M - V$ and $u_L - V$, derived from the principles of mixture theory [19, 24], in order to define the effective velocity V of the mixture. The role of the diffusion coefficients $D_M, D_L > 0$ is precisely to make the mixture more homogeneous by imposing mass transfer by diffusion. Note that the bulk velocity is divergence free when the mixture is made of one constituent only ($M = 0$ or $M = 1$); otherwise compressibility is driven by the difference $D_M - D_L$.

For the continuous equations, we can work equivalently with (1), (2), (3), (4) or (1), (2), (4), (5). We complete the system by an initial condition $M|_{t=0} = M_0$ and boundary conditions on $\partial\Omega$, that will be detailed later on.

Remark 2.1. Since in general $\nabla_X \cdot V \neq 0$, it could be relevant to add in the Stokes equation (4) the term $\nabla_X(\lambda \nabla_X \cdot V)$ with a viscosity coefficient $\lambda \geq 0$ that is required to satisfy some compatibility relation with μ . Here, we simply set $\lambda = 0$, which is always admissible.

2.2. Parameter settings

Our model involves several quantities having typical front-like behavior, that we model with sigmoidal functions. We set

$$\Sigma_P^+(x) = (p_{max} - p_{min}) \frac{x^{2\alpha_p}}{x^{2\alpha_p} + \chi_p^{2\alpha_p}} + p_{min} \quad \text{and} \quad \Sigma_P^-(x) = (p_{max} - p_{min}) \left(1 - \frac{x^{2\alpha_p}}{x^{2\alpha_p} + \chi_p^{2\alpha_p}} \right) + p_{min} \quad (7)$$

which depend on a set of 4 parameters embodied into the shorthand notation $P = (p_{max}, p_{min}, \alpha_p, \chi_p)$. We see that Σ^+ (resp. Σ^-) is an increasing (resp. decreasing) sigmoidal function with limit values $p_{min} < p_{max}$, χ_p is the inflexion point and α_p modulates the transition slope.

Firstly, let us discuss the form of the viscosity distribution. We suppose that the mucus is more viscous than the luminal content and that there exists a concentration threshold that completely changes the rheological properties of the fluid. We then model the function μ with the parameters $P_\mu = (\mu_{max}, \mu_{min}, \alpha_\mu, \chi_\mu)$ and the sigmoidal function

$$\mu(M)(x, y) = \Sigma_{P_\mu}^+(M(x, y)).$$

Secondly, we focus on the diffusion coefficients D_M and D_L . Those diffusion coefficients may depend on the local composition of the mixture, but are also strongly determined by spatial features, such as the microscopic structure of the mucus gel and of the gut wall. In order to avoid additional non linearities and regarding the lack of precise knowledge of the links between mucus concentration, mucus layer microscopic structure and effective diffusion, we chose to only consider spatial dependence of the diffusion by introducing specific modelling assumptions. Some perspectives to improve the model on that issue will be given in the last section. We suppose that the mucus layer is confined near the mucosa. Consequently, the correction tuned by D_M should be small near $\Gamma_l \cup \Gamma_r$ and high at the center of the domain, and reversely for D_L . We also suppose that D_M and D_L are uniform with respect to y . Denoting $P_K = (D_{K,max}, D_{K,min}, \alpha_K, \chi_K)$ with $K \in \{L, M\}$, we set

$$D_L(x, y) = \Sigma_{P_L}^+(x) \quad \text{and} \quad D_M(x, y) = \Sigma_{P_M}^-(x).$$

Thirdly, we assume that the mucus is initially essentially located near the mucosa with a sharp transition; given $P_{M_0} = (M_{0,max}, M_{0,min}, \alpha_{M_0}, \chi_{M_0})$, it leads to define

$$M_0(x, y) = \Sigma_{P_{M_0}}^+(x). \quad (8)$$

3. DISCUSSION ON THE BOUNDARY CONDITIONS

We face different modelling issues concerning boundary conditions. We remind the reader that the different boundaries of the domain describe completely different physiological functions. On the one hand, the lateral boundaries $\Gamma_l \cup \Gamma_r$ represent the intestinal mucosa which produces mucus and pumps luminal liquid, influencing both mass conservation and flow speeds. On the other hand, the horizontal boundary conditions on Γ_{in} and Γ_{out} have to model free inflow and outflow of matter.

3.1. Boundary conditions for $\Gamma_l \cup \Gamma_r$

On the lateral boundaries, the flux is driven by mucus production and liquid pumping according to

$$(MV - D_M \nabla_X M) \cdot \vec{n} = -f_M(M) \quad \text{and} \quad (LV - D_L \nabla_X L) \cdot \vec{n} = -f_L(L), \quad (9)$$

Mucus production and water pumping depend on certain thresholds: we set

$$f_M(M) = \theta_M [M - M_*]^- , \quad f_L(L) = -\theta_L [L - L_*]^+ .$$

The former means that the mucosa produces at rate θ_M when the mucus concentration is below the threshold M_* , while the latter tells us that the mucosa pumps liquid at rate θ_L only when the liquid concentration is above the threshold L_* . A linear combination of (9), together with (1), yields $\left(M + \frac{D_M}{D_L} L\right) V \cdot \vec{n} = -f_M - \frac{D_M}{D_L} f_L$. It implies a Dirichlet boundary condition for the transverse velocity u . We can freely define v on $\Gamma_l \cup \Gamma_r$ without influencing the normal flow of M and L . Keeping in mind compatibility conditions at the corners of the domain, we impose that the tangential velocity vanishes. We arrive at

$$V \cdot \vec{n} = u = -\frac{f_M + \frac{D_M}{D_L} f_L}{M + \frac{D_M}{D_L} L} \quad \text{and} \quad V \cdot \vec{\tau} = v = 0. \quad (10)$$

3.2. Boundary conditions for Γ_{in} and Γ_{out}

The definition of relevant boundary conditions on Γ_{in} and Γ_{out} is more challenging. We assume that diffusion does not contribute to fluxes at the inflow and outflow boundaries:

$$D_M \nabla_X M \cdot \vec{n} = 0 \quad \text{and} \quad D_L \nabla_X L \cdot \vec{n} = 0. \quad (11)$$

The boundary conditions for the velocity have a crucial role on the behaviour of the model: by constraining the velocity field, they drive the mucus displacement and its equilibrium with the liquid inside the domain. The boundary conditions should produce a stable mucus layer without over constraining the system in a non physiological way. Choosing Dirichlet boundary conditions at Γ_{in} is relevant since the average fluid intake into the gut is a known biological parameter. As the intestinal flow is mainly longitudinal, it might be natural, at first sight, to assume that the transverse velocity is null on this boundary. On the contrary, relaxing the constraint on Γ_{out} is meaningful because we want to investigate the model response to the inflow only. For that reason, we choose a no-strain boundary condition. We then get

$$u = 0 \quad \text{and} \quad v = v_{in} \quad \text{on } \Gamma_{in} \quad \text{and} \quad (\mu(M) (\nabla_X V + \nabla_X V^T) - PId) \vec{n} = 0 \quad \text{on } \Gamma_{out} \quad (12)$$

Remark 3.1. The numerical simulations in Section 5.1 show that the no-strain condition on Γ_{out} could produce questionable velocity and mucus distribution profiles in the vicinity of Γ_{out} , likely due to the use of the symmetric strain rate tensor in the no-strain boundary condition. We made a few attempts with Dirichlet conditions, taking into account the corresponding compatibility conditions for the Stokes equation; however they produce irrelevant velocity profiles next to the boundary. Possible improvements of the condition can also be found in [2–4].

3.3. Derivation of an approximated profile for v_{in} .

We wish to capture steady-states with mucus layers next to the lateral boundaries. Accordingly, since the viscosity μ has a sharp profile as a function of M , strong variations of the velocity are expected in this region too. The boundary conditions on Γ_{in} should reflect this behavior in order to avoid too strong correction of the velocity field near Γ_{in} . We will discuss several options to obtain such a relevant profile for (u_{in}, v_{in}) , compatible with the expected steady-states. One of them consists in deriving an approximation of the inflow.

To this end, we find a reduced model based on asymptotic reasoning. We rewrite the equations in dimensionless form and we make the aspect ratio $\varepsilon = \frac{L_x}{L_y}$ appear. It turns out that the regime $0 < \varepsilon \ll 1$ is relevant for our purposes. We seek solutions as an expansion in power series of ε , where for the velocity the leading term has the form $(\varepsilon u_1, v_0)$. A specific regime of the pressure characteristic value leads to an explicit formulation of v_0 , which links the velocity with the viscosity distribution and the boundary conditions. As we specifically focus on the case of a sharp mucus layer located near the mucosa in the vicinity of Γ_{in} , we approximate the corresponding viscosity profile with the step function $\tilde{\mu} = \mu_{min} \mathbf{1}_{(0, R_m)} + \mu_{max} \mathbf{1}_{(R_m, 1)}$ for a certain $0 < R_m < 1$ (in dimensionless units). We introduce $\tilde{\mu}$ in the explicit formulation of v_0 , which gives the following formal approximation for the longitudinal velocity on Γ_{in}

$$v_{in}(x) = \frac{w_{in}}{\gamma} \left(\frac{1-x^2}{2\mu_{max}} \mathbf{1}_{(R_m, 1)}(x) + \left(\frac{1-R_m^2}{2\mu_{max}} + \frac{R_m^2-x^2}{2\mu_{min}} \right) \mathbf{1}_{(0, R_m)}(x) \right), \quad (13)$$

where

$$\gamma = \frac{1}{8} \left(\frac{1}{\mu_{min}} R_m^4 + \frac{1}{\mu_{max}} (1 - R_m^4) \right),$$

with given $w_{in} > 0$, $0 < R_m < 1$. The simplified asymptotic model of the flow (i.e. $(\varepsilon u_1, v_0)$) will be used for the sensitivity analysis in Section 6 since it permits us to reduce the computational cost.

4. NUMERICAL SCHEME

We update the mucus volume fraction with (2), the velocity-pressure pair is determined by the system (4)–(5) while the luminal liquid volume fraction L is simply defined by (1). We choose a semi-implicit scheme so that the computation of the volume fractions and the velocity–pressure fields are decoupled. We work with Cartesian grids and we use well-established schemes for both equations. The diffusion term in (2) is treated by the VF4 method, which is known to converge on meshes satisfying the orthogonality condition, such as Cartesian grids [9, Sect. 3.1.1]. The transport term is approached according to UpWind principles. The Stokes system is dealt with by using the MAC scheme, which dates back to [12]. Accordingly, pressure, horizontal, and vertical velocities are evaluated on staggered grids; the volume fraction M is stored on the same grid as the pressure, see Fig. 1b. We refer to the grid cells and the corresponding unknowns with the notations $\Omega_{i,j}$ (for P , M grid), $\Omega_{i-\frac{1}{2},j}$ (for u) and $\Omega_{i,j-\frac{1}{2}}$ (for v).

The Finite Volume framework mimics the formulae obtained by integrating the equations over the grid cells. For instance, for the horizontal velocity we get

$$\int_{\partial\Omega_{i-\frac{1}{2},j}} \mu(M) (\nabla_X V + \nabla_X V^T) \cdot \vec{n} \, d\omega - \int_{\Omega_{i-\frac{1}{2},j}} \partial_x P \, d\Omega = 0 \quad (14)$$

where \vec{n} is a outward normal vector to the boundary of $\Omega_{i-\frac{1}{2},j}$. The boundary integral splits as a sum over the edges. The staggered grids allow us to evaluate the derivatives by mere finite differential quotients. We are led

to the following discrete equivalent to (14)

$$\begin{aligned}
 & -\Delta x \tilde{\mu}_{i-\frac{1}{2},j-\frac{1}{2}} \left(-\frac{u_{i-1/2,j} - u_{i-1/2,j-1}}{\Delta y} - \frac{v_{i,j-1/2} - v_{i-1,j-1/2}}{\Delta x} \right) - \Delta y \mu(M_{i,j}) \left(2\frac{u_{i+1/2,j} - u_{i-1/2,j}}{\Delta x} \right) \\
 & -\Delta x \tilde{\mu}_{i-\frac{1}{2},j+\frac{1}{2}} \left(\frac{u_{i-1/2,j+1} - u_{i-1/2,j}}{\Delta y} + \frac{v_{i,j+1/2} - v_{i-1,j+1/2}}{\Delta x} \right) + \Delta y \mu(M_{i-1,j}) \left(2\frac{u_{i-1/2,j} - u_{i-3/2,j}}{\Delta x} \right) \\
 & + \Delta x \Delta y \frac{P_{i,j} - P_{i-1,j}}{\Delta x} = 0.
 \end{aligned} \tag{15}$$

The quantities $\tilde{\mu}$ are not directly defined since M , and thus μ , is not stored at the interfaces $i + \frac{1}{2}, j + \frac{1}{2}$, where it needs to be reconstructed. For instance we can use the mean value $\tilde{M}_{i+\frac{1}{2},j+\frac{1}{2}} = \frac{1}{4}(M_{i,j} + M_{i,j+1} + M_{i+1,j} + M_{i+1,j+1})$. When the viscosity has a sharp profile, it can be more efficient to reconstruct $\tilde{\mu}_{i+\frac{1}{2},j+\frac{1}{2}}$ by the harmonic mean [9, Sect. 2.3]. We proceed similarly with the vertical velocity, integrating the second component of Eq. (4). Finally integrating (5) over $\Omega_{i,j}$ leads to

$$\Delta x (v_{i,j+1/2} - v_{i,j-1/2}) + \Delta y (u_{i+1/2,j} - u_{i-1/2,j}) = \mathcal{D}_{i,j} \tag{16}$$

where $\mathcal{D}_{i,j}$ is the approximation of the diffusion flux $\int_{\partial\Omega_{i,j}} (D_M - D_L) \nabla_X M \cdot \vec{n} \, d\omega$ defined by the VF4 formalism [9]. The same numerical flux is used to update M through the discretization of (2) where the convection term is obtained with explicit upwind fluxes, while the diffusion term is treated implicitly.

The boundary conditions are discretized differently according to the boundary and the equation under consideration. The convection–diffusion equation for M is complemented either by the Robin condition (9), with a convection flux given on Γ_r, Γ_l by (10), or the Neumann condition (11) on $\Gamma_{in}, \Gamma_{out}$ with a convection flux given by (12).

On the boundaries Γ_l, Γ_r (resp. Γ_{in}), the treatment of the equations involving non–interior values for u, v and M is rather standard. The velocities are determined by using the Dirichlet boundary condition (10), while for the volume fraction we use the Robin-like (resp. Neumann) condition in (9) (resp. (11)) to define the missing M 's.

On Γ_{out} the viscous fluxes vanish by virtue of (12). The diffusion fluxes for M are also set to 0 due to (11). The only difficulty comes when evaluating the vertical velocity. To this end, we integrate the second component of Eq. (4) in half a grid cell and we introduce ghost points, as shown in Fig. 1c. We observe that three contributions on the boundaries of the cell vanish thanks to the boundary condition (12); the fourth boundary on the top gives an equation for v on such boundary cells $\Omega_{i,j-1/2}$.

5. NUMERICAL RESULTS

For the numerical experiments, the computational domain is $\Omega_D = [-L_x, L_x] \times [-L_y, 0]$, with $L_x = 2, L_y = 12$ (in *cm*) and we work with 100×300 grid points that define square cells. The parameters of the model are given in Table 1. We shall comment the role of the conditions on Γ_{in} and Γ_{out} and discuss numerical experiments where a stable mucus layer establishes.

5.1. Comments on the boundary conditions

As explained in Remark 3.1, it is likely that the velocity imposed on Γ_{in} plays a crucial role in the formation of the mucus layer, and a certain compatibility should be satisfied between the expected steady state and the incoming field (u_{in}, v_{in}) . If no measurements are available, we can start with the profile (13) (and $u_{in} = 0$) which is based on an asymptotic argument. According to the intuition, the velocity field is quite uniform in the vertical direction, see Fig. 3a for an overview of the horizontal speed over the whole domain. It suggests that the condition on Γ_{in} can be improved with the following iterative procedure: a) Define (u, v) by solving the system (4)–(5), b) set $(u_{in}, v_{in})(x) = (u, v)(x, -\frac{L_y}{2})$ and go back to step a). This approach can also be justified

Name	Meaning	Unit	Sigmoidal distribution				Other value
			p_{max}	p_{min}	α_p	χ_p	
D_L	Liquid diffusion	$\text{cm}^2 \text{day}^{-1}$	$2.5 \cdot 10^{-3}$	10^{-4}	16	$\frac{3}{4}L_x$	-
D_M	Mucus diffusion	$\text{cm}^2 \text{day}^{-1}$	10^{-5}	10^{-6}	12	$\frac{3}{4}L_x$	-
μ	Viscosity	Pa.s	$1.97 \cdot 10^{-2}$	10^{-3}	7	0.4	-
M_0	Initial mucus distribution	\emptyset	0.98	0	15	$\frac{3}{4}L_x$	-
θ_M	Mucus production rate	day^{-1}		-			10^{-3}
M_*	Mucus production threshold	\emptyset		-			0.98
θ_L	Water pumping rate	day^{-1}		-			5
L_*	Water pumping threshold	\emptyset		-			0.2
w_{in}	Average input speed (simplified model)	cm day^{-1}		-			-80

TABLE 1. Biophysical constants of the model. Sigmoidal distribution is defined with Eq. (7). The parameters p_{max} and p_{min} are the maximal and minimal bounds of the sigmoid, α_p its slope and χ_p its inflexion point. We emphasize that the diffusion parameters for the liquid and the mucus are respectively of order $10^{-12}\text{m}^2\text{s}^{-1}$ and $10^{-14}\text{m}^2\text{s}^{-1}$, in order to mimic the diffusion of large molecules —such as polysaccharides— in highly viscous media — such as the chyme and the mucus. They remain in documented orders of magnitude for large molecule diffusions in mucus [15].

by the fact that we are only considering a relatively short portion of the gut. Note that we have two choices for u_{in} thereafter, namely we can set $u_{in} = 0$ as before or we can use the function u_{in} given as a result of the iterative procedure.

Fig. 2 compares the velocity profiles with 0 or 1 iteration of the iterative procedure at $y = -\frac{L_y}{2}$, far away from Γ_{in} so that the influence of the Dirichlet condition may be moderate, and at $y = -\frac{\Delta y}{2}$ where boundary-layer effects can be sensitive. We pay a specific attention to the role of u_{in} . As far as we consider the vertical component v of the velocity, the resulting profiles are quite similar between two consecutive iterations of the iterative procedure, and quite close to the formal approximation given by Eq. (13) (the maximal relative difference is 5%) including next to Γ_{in} , see Fig. 2a. Conversely, if we use an alternative iteration procedure to define v_{in} only, but keeping $u_{in} = 0$, very slight discrepancies are observed on u at $-L_y/2$, but boundary-layer effects are clearly sensitive next to Γ_{in} , see Fig. 2b and 2d : we observe oscillations with high amplitude which might create instabilities. Those oscillations are two orders of magnitude higher during the iteration 0 than the iteration 1. This discussion reveals that the choice of (u_{in}, v_{in}) is certainly far from harmless.

As said in Section 3.2, the condition (12) on Γ_{out} is questionable. We see the effect of the boundary condition on Fig. 3: significantly larger horizontal velocities appear in the vicinity of Γ_{out} . The spurious velocities are oriented from the lumen of the gut to the wall. Consequently, a part of the mucus near Γ_{out} will be washed-out, as it can be observed on the mucus profile on Fig. 3c after five days: close to Γ_{out} the layer of mucus is smaller than inside the domain. Nevertheless, the flow is mostly oriented outward and, as confirmed by these results, the effects of the null strain boundary condition remain confined close to the boundary.

5.2. Stable steady-state mucus layer

In order to evaluate the robustness of the model, we compare the large-time state of the flow when we start from the sigmoidal state (8), here denoted $M_{0,s}$, or from a Gaussian distribution

$$M_{0,g}(x, y) = M_{max} \left(\exp \left(-\frac{(x - L_x)^2}{2 \left(\frac{L_x}{6}\right)^2} \right) + \exp \left(-\frac{(x + L_x)^2}{2 \left(\frac{L_x}{6}\right)^2} \right) \right).$$

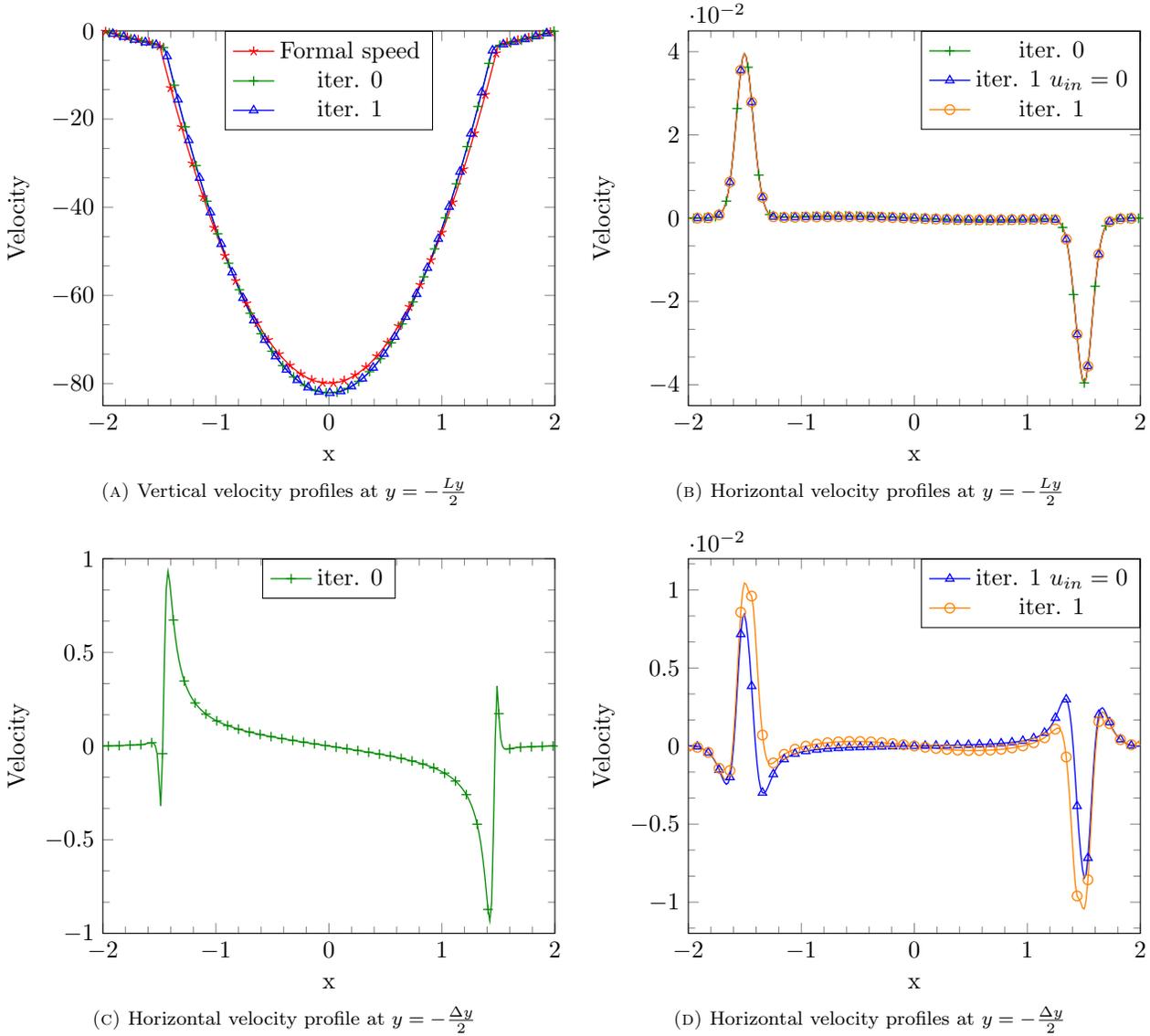


FIGURE 2. Speed profiles at $y = -\frac{Ly}{2}$ and $y = -\frac{\Delta y}{2}$ for the first iterations of the iterative procedure defined in Sec. 5.1. The formal speed designates the boundary conditions (13) used for the initialization of the iterative procedure. The notation $u_{in} = 0$ stands for the result of the alternative iterative procedure keeping $u_{in} = 0$. We had to displayed the horizontal velocity profiles at $y = -\frac{\Delta y}{2}$ for iter.0 and iter.1 on different plots, due to their different order of magnitude.

For both initial conditions, we perform the same simulations, with the boundary condition (13) for v_{in} . After 60 days the two mucus profiles coincide, see Fig. 4b (in the area where the mucus volume fraction is larger than $\frac{1}{100}$ the relative difference on the profiles is about 2%). The mucus layer and its shape are thus not strongly determined by the initial condition, at least in these configurations. However, if we use the iterative procedure

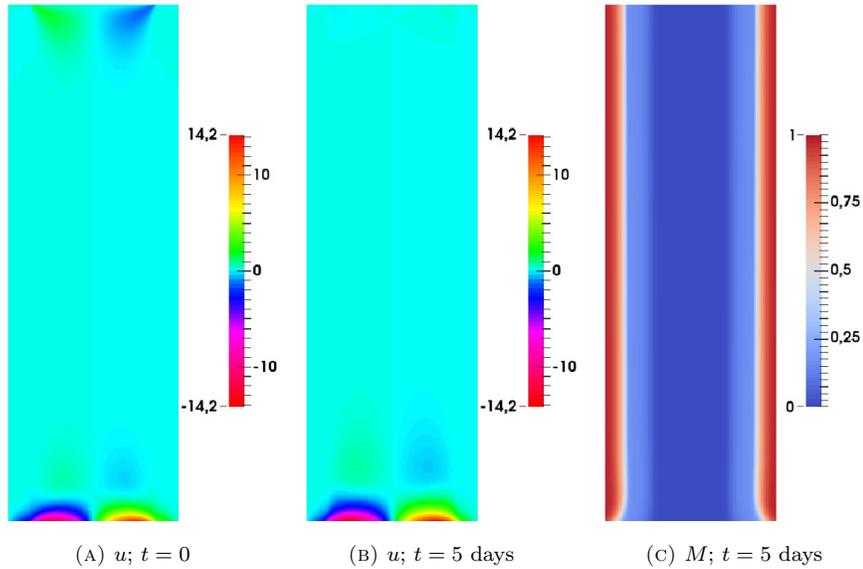


FIGURE 3. Horizontal speed u and mucus M distributions at $t = 0$ or $t = 5$.

to compute v_{in} , the profile v_{in} depends on the initial data for M and some discrepancies on the mucus profile at larger times appear; see Fig. 5 for a comparison between the sigmoidal and the Gaussian profiles.

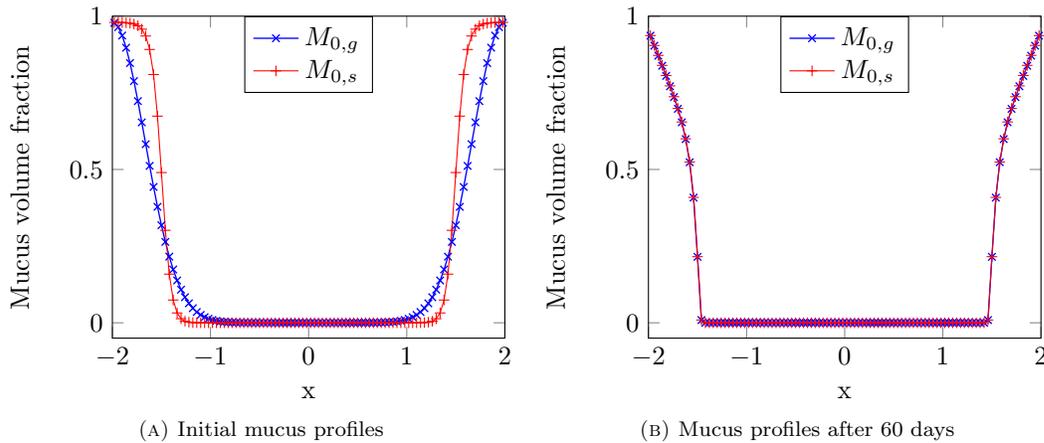


FIGURE 4. Mucus profiles at $y = -\frac{L_y}{2}$ for initial data $M_{0,g}$ and $M_{0,s}$ at $t = 0$ and $t = 60$ days with v_{in} given by Eq. (13).

We also investigate the ability of the model to recover its steady states when the mucus layer is strongly perturbed at $t = 0$. We start from the sigmoidal shape $M_{0,s}$, and we compute the condition on Γ_{in} with the iterative procedure. Once the boundary condition is determined, we reset the initial condition by eroding the mucus layer between $y = -4\text{cm}$ and $y = -9\text{cm}$. Namely, in this domain we modify the parameter of the sigmoid, changing only the inflexion point. Fig. 6 displays several snapshots of the evolution of the volume fraction M . The mucus layer disruption is neatly visible at $t = 0$: we note $M_{0,p}$ that initial perturbed distribution. After

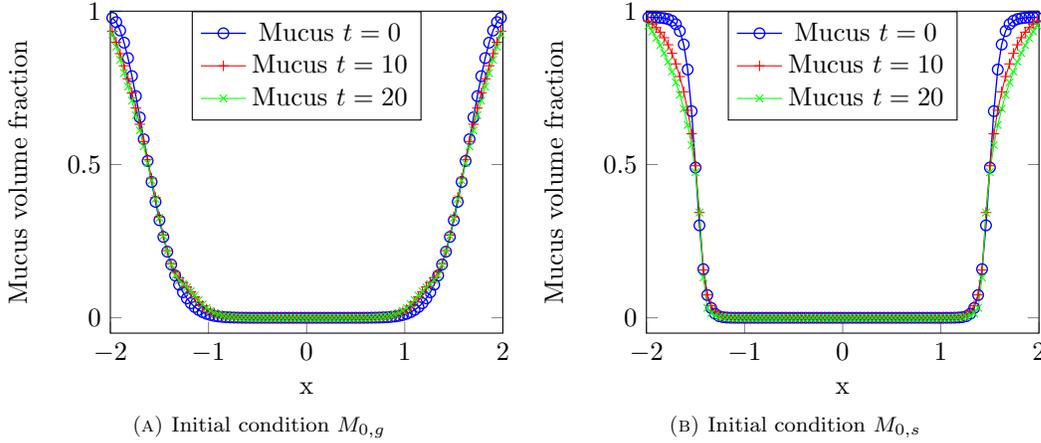


FIGURE 5. Mucus profiles at $y = -\frac{L_y}{2}$ for initial data $M_{0,g}$ and $M_{0,s}$ at $t = 0, 10$ and $t = 20$ days with v_{in} given by the iterative procedure.

one day, a tongue of mucus is transported from uphill and starts to overlay the eroded mucus layer area. The initial disruption is also transported and its downhill part is abraded by the liquid flow. At $t = 2$ days, half of the initial disrupted zone has been already transported outside the domain and the mucus tongue increases until re-covering a mucosa portion equivalent to the initial disruption. At $t = 3$ days, the mucus tongue reaches Γ_{out} and at $t = 5$ days, the recovering is quasi-completed. During the whole simulation, the mucus layer located upstream is stable. The final mucus layer is visually equivalent to the layer of the unperturbed data.

The first plot of Fig. 7 represents the mucus profile at $y = -8\text{cm}$ at the same days than in Fig. 6. At $t = 5$, we also plot the mucus profile at $y = -3\text{cm}$ for comparison issues. At $t = 1$, we can see that the mucus layer is still disrupted. Then, at $t = 2$ and $t = 3$, the mucus tongue appears, exhibiting a few mucus peaks. The peaks grow to fill up the mucus layer until reaching the steady state at $t = 5$ days. The luminal part of the mucus tongue is superimposed with the steady state mucus profile at $t = 5$ and $y = -3\text{cm}$. The second plot of Fig. 7 displays the time evolution of the L^2 norm of the difference between the current volume fraction of mucus and the volume fraction at the previous day. This quantity rapidly drops down until reaching a steady-state at about $t = 10$ days, indicating that the mucus volume fraction is in a stationary regime. This numerical experiment shows the recovering dynamics of the mucus layer after degradation and proves the ability of the model to preserve and restore a stable mucus layer.

6. SENSITIVITY ANALYSIS

In order to better interpret the mechanisms involved in the formation of a stable mucus layer, we perform a sensitivity analysis of the model to identify the parameters that most impact the shape of the mucus layer at steady-state. The sensitivity analysis starts by choosing uncertain model parameters; they are modelled as random variables with suitable probability distributions. We then sample these random parameters and run the deterministic model for each realization. Finally, we quantify with appropriate statistics the induced variability of relevant descriptors of the mucus layer shape. In order to reduce the computational load, we use the reduced model presented in Section 3.3.

This model has 21 parameters: for computational reasons, all the parameters cannot be tested all together. We choose to focus on the threshold effects related to the sigmoidal shape of the coefficients and initial condition: we select the initial mucus front location χ_{M0} , the diffusion coefficient transition location χ_M , the mucus production rate θ_M , the liquid pumping rate θ_L , the viscosity transition χ_μ and the input speed w_{in} . As we

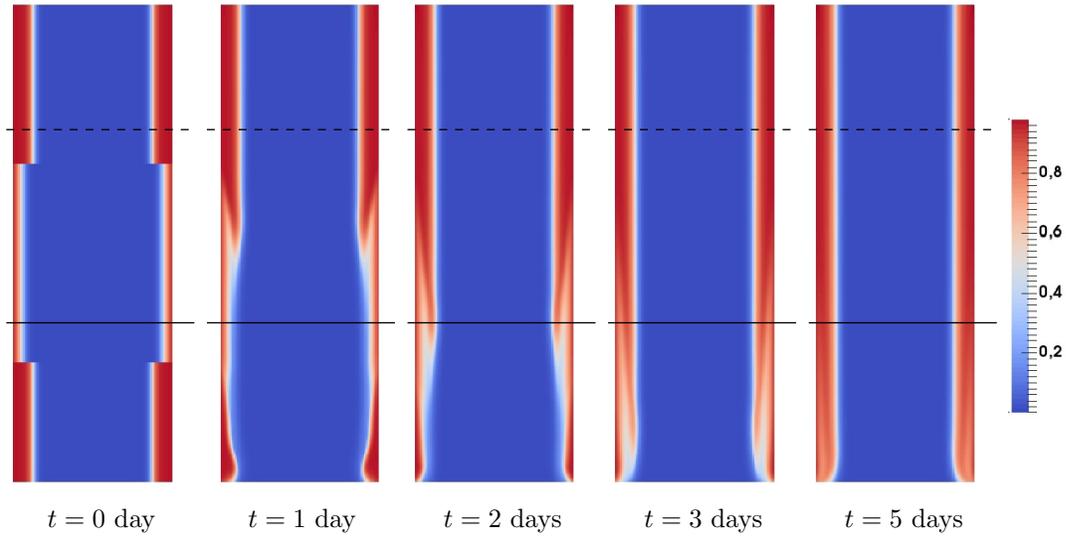


FIGURE 6. Evolution in time of the disrupted mucus layer. We present the mucus volume fraction map at different times in order to illustrate the reconstitution of the steady-state mucus layer. The plot $t = 0$ displays $M_{0,p}$, the initial perturbed distribution. The dashed and continuous lines represent respectively the lines $y = -3\text{cm}$ and $y = -8\text{cm}$.

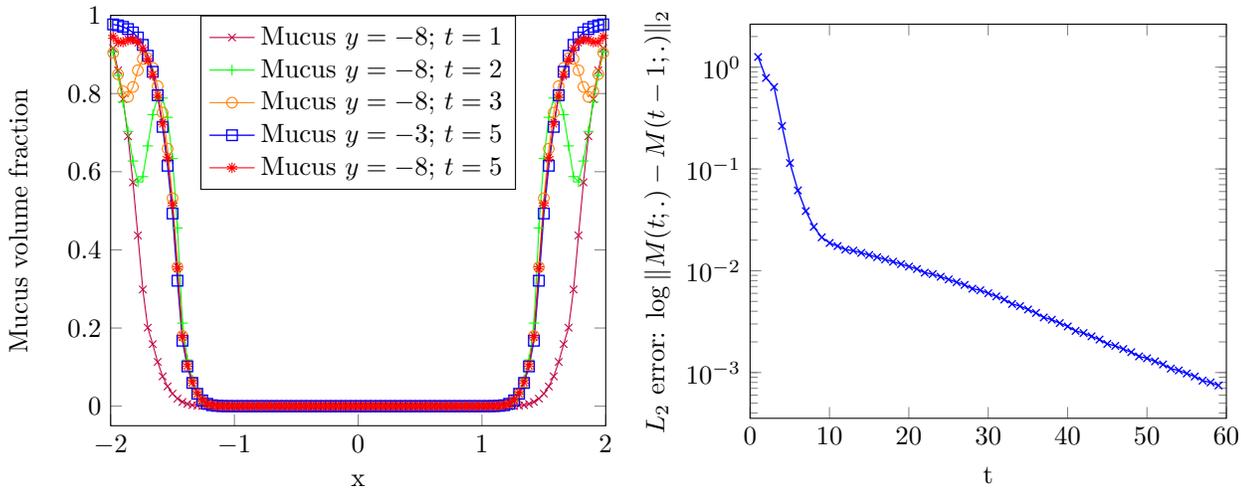


FIGURE 7. Left plot: mucus profile at $y = -3\text{cm}$ or $y = -8\text{cm}$ at different times. Right plot: evolution in time of $\log \|M(t; \cdot) - M(t-1; \cdot)\|_2$.

have no prior physiological knowledge on the variability of the parameters, we use uniform random variables. The mean values are given by Table 1; the standard deviation is chosen as 25 % of the mean value. We ran the deterministic code until steady-state, with maximal simulation time of 20 days, which is enough to stabilize the mucus layer. Assuming that the mucus layer is uniform in y , we look for suitable descriptors of its shape. This is done by computing the parameters of the sigmoidal function $f_{obs}(x, y) = (\max_{obs} - \min_{obs}) \frac{x^{2\alpha_{obs}}}{x^{2\alpha_{obs}} + \chi_{obs}} + \min_{obs}$

that best fits the steady-state mucus profile in the least-square sense. These parameters are used as observables in our sensitivity analysis.

As we want to minimize the number of runs of the deterministic code, we choose the non-intrusive pseudo-spectral method of generalized Polynomial Chaos (gPC), an extension of the method developed in [7]. The numerical output $\Upsilon = (\max_{obs}, \alpha_{obs}, \chi_{obs}, \min_{obs})$ is decomposed on a basis of orthogonal Polynomial Chaos depending on the spatial variable X and on the uncertain input $\xi(\omega) = (\chi_{M0}, \chi_M, \theta_M, \theta_L, \chi_\mu, w_{in})$, where ω is the corresponding vectorial probability density. Namely, we compute the deterministic coefficients (a_j) with orthogonal projections, in order to get

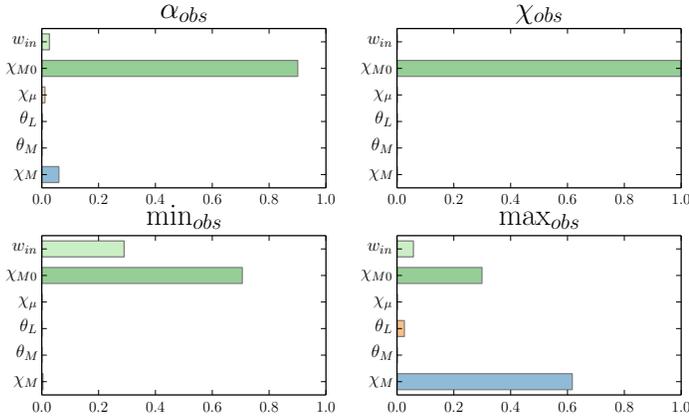
$$\Upsilon(x, \omega) = \sum_{j=1}^M a_j(x) \psi_j(\xi(\omega)), \quad \text{with} \quad a_j(x) = \mathbb{E}[\Upsilon, \psi_j(\xi(\cdot))], \quad \forall j \in \{1, \dots, M\} \quad (17)$$

where $\{\psi_j\}_j$ are the Polynomial Chaos basis of order at most p . For uniform distributions, a suitable ω -orthonormal basis is the Legendre polynomials. For our purpose, a degree $p = 3$ is sufficient for the convergence of statistical results. The bottle-neck of the method relies in the estimation of the multidimensional integrals with probability support ω needed to compute the coefficients a_j . When the number of uncertain parameters N is low ($N < 4$), efficient high-order numerical quadratures of full-tensor products [8] represent an appropriate alternative to Monte-Carlo type sampling which are computationally expensive. For higher dimensions, full quadrature grids have also a prohibitive computational load. We then use sparse grid quadrature [10] which takes advantages of sound partial tensorizations, avoiding the combinatorial explosion of the sample size while keeping a high level of accuracy. Consequently, the expansion coefficients have been estimated based on a Clenshaw-Curtis (CC) sparse cubatures of level 5 [17]. With this choice, we made 389 runs of the deterministic code in total for $N = 6$. To quantify the sensitivity of the outputs to the input uncertainty, we compute two statistical indicators. We first determine the output coefficients of variation $\Upsilon_{i,CV} = \Upsilon_{i,std}/\Upsilon_{i,mean}$. Next, we compute the Sobol's indices [22] which estimate the contribution of each parameter, or groups of parameters, to the total variability of Υ . They are based on a normalization of the values $V_i = Var(E[\Upsilon|\xi_i])$, resp. $V_{ij} = Var(E[\Upsilon|\xi_i, \xi_j]) - V_i - V_j$, which evaluates the magnitude of the variability of the output subject to variations of the parameter i , resp. of the parameters i and j . The first and second order Sobol's indices then read $S_i = V_i/Var(\Upsilon)$ and $S_{ij} = V_{ij}/Var(\Upsilon)$.

We start by checking the first order Sobol's indices. The results are presented in Fig. 8a and Table 8b. The coefficients of variation first indicate that the maximal value of the sigmoidal output has very small variations, unlike the other parameters. This variability is partially explained by the occurrence of extremal cases such as filling up of the entire domain by the mucus. The Sobol's indices show that the parameter χ_{M0} is strongly predominant on the variability of all the observables except \max_{obs} . It suggests that our model is strongly determined by its initial value. We then perform another analysis by fixing the parameter χ_{M0} to its mean value, in order to analyse the influence of the remaining parameters. see Fig. 9a and Table 9b. The coefficients of variation of the observables are low, except for the slope of the sigmoid, indicating that the parameter variations modify the magnitude of the mucus gradient rather than radially transporting a sharp mucus front. It also suggests that the extremal cases are much less frequent when χ_{M0} is fixed. The Sobol's indices inspection shows that χ_M is the most influential parameter on the whole set of observables, followed by the input speed w_{in} and the crossed contribution of w_{in} and χ_M . At the other side of the spectrum, θ_M is the weakest contributor to the output variability. These values reflect the diffusion and convection interplays during the determination of the large time solution. We note that the parameters that drive the boundary conditions or the threshold of the viscosity function have less impact on the outcomes of that model.

7. INTERACTION WITH A POPULATION OF CHEMOTACTIC BACTERIA

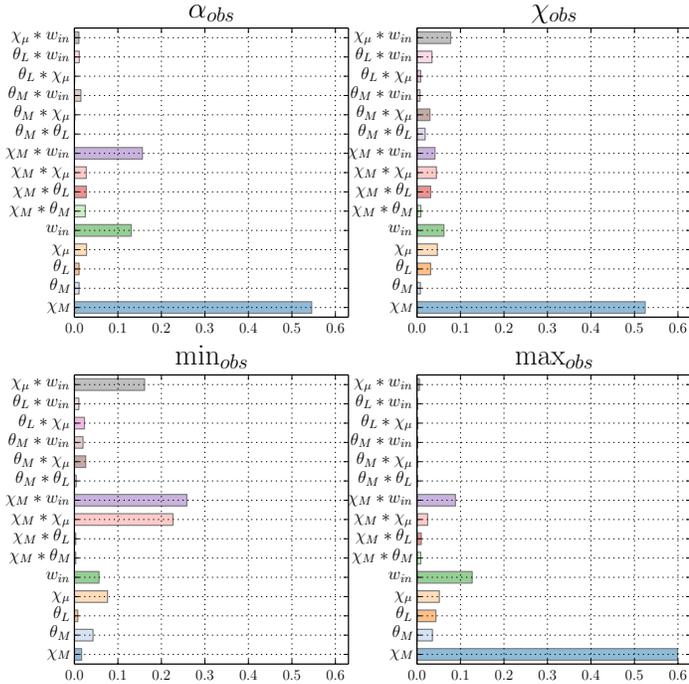
We now propose an extension of the model by taking into account the presence of the bacterial community. Our modelling is definitely rough and questionable, but it already allows us to bring out interesting features.



(A) Bar plot of Sobol indices.

	\max_{obs}	α_{obs}	χ_{obs}	\min_{obs}
χ_M	0.6167	0.0602	0.0001	0.004
θ_M	0.0001	0.0000	0.0000	0.0000
θ_L	0.0259	0.0009	0.0004	0.0000
χ_{M0}	0.2991	0.9007	0.9991	0.7056
χ_μ	0.0005	0.0112	0.0003	0.0003
w_{in}	0.0577	0.0270	0.0000	0.2899
CV	0.0034	0.8470	0.4931	1.6544

(B) Table of Sobol indices and coefficient of variations.

FIGURE 8. Bar plot and table of the Sobol indices for each observable. The notation χ_M corresponds to S_i where i is the index of χ_M in ξ .

(A) Bar plot of Sobol indices.

	\max_{obs}	α_{obs}	χ_{obs}	\min_{obs}
χ_M	0.5990	0.5454	0.5246	0.0165
θ_M	0.0355	0.0107	0.0078	0.0427
θ_L	0.0435	0.0107	0.0314	0.0078
χ_μ	0.0514	0.0279	0.0469	0.0761
w_{in}	0.1269	0.1307	0.0620	0.0565
$\chi_M * \theta_M$	0.0087	0.0252	0.0089	0.0031
$\chi_M * \theta_L$	0.0099	0.0275	0.0315	0.0030
$\chi_M * \chi_\mu$	0.0246	0.0274	0.0447	0.2267
$\chi_M * w_{in}$	0.0885	0.1563	0.0414	0.2585
$\theta_M * \theta_L$	0.0007	0.0000	0.0187	0.0041
$\theta_M * \chi_\mu$	0.0011	0.0008	0.0298	0.0259
$\theta_M * w_{in}$	0.0011	0.0149	0.0070	0.0197
$\theta_L * \chi_\mu$	0.0018	0.0005	0.0086	0.0231
$\theta_L * w_{in}$	0.0008	0.0112	0.0345	0.0102
$\chi_\mu * w_{in}$	0.0057	0.0103	0.0774	0.1613
CV	0.0140	1.9338	0.0167	0.0000

(B) Table of Sobol indices and coefficient of variations.

FIGURE 9. Bar plot and table of the Sobol indices for each observable. The notation χ_M and $\chi_M * \theta_M$ correspond respectively to S_i and S_{ij} where i and j are the respective indices of χ_M and θ_M in ξ .

We gather all the bacterial community in a single population considered as an additional phase in the mixture

model with volume fraction $B(t, X)$. It obeys a convection–diffusion equation with external potential ϕ

$$\partial_t B + \nabla_X \cdot (BV - B\nabla_X \phi) = \nabla_X \cdot (D_B \nabla_X B) \tag{18}$$

and the volume conservation condition becomes $B + L + M = 1$. The space-dependent diffusion coefficient D_B is intended to model both the own bacterial diffusion and interphases interactions. Additionally, the displacement of the bacteria is driven by a chemotactic potential ϕ . Velocity and pressure are defined by Stokes Eq. (4) with the appropriate boundary conditions, and the constraint

$$\nabla_X \cdot V = \nabla_X \cdot ((D_B - D_L) \nabla_X B + (D_M - D_L) \nabla_X M + B \nabla_X \phi). \tag{19}$$

Two different biological phenomena are embodied into the potential ϕ : 1) the bacteria are supposed to be attracted by the mucus, they are “attached” to this viscous fluid to resist against the luminal liquid wash out and to take advantage of this nutrient source; 2) conversely, bacteria cannot penetrate too deeply into the mucus, since they are attacked by the immune system of the host. We phenomenologically account for these phenomena by introducing an attracting rate $f(M)$ which is optimal when the volume fraction of mucus reaches the threshold M_{ref} . The chemotactic potential is then defined through the Poisson equation

$$\Delta_X \phi = f(M) - \frac{1}{|\Omega|} \int_{\Omega} f(M) dX, \quad \text{with} \quad f(M) = 1 - \frac{1}{\eta (M - M_{ref})^2 + 1} \quad (\eta > 0). \tag{20}$$

This equation is supplemented by homogeneous Neumann boundary conditions and we select the solution verifying $\int_{\Omega} \phi dX = 0$. We close the system with an initial condition B_0 and the following boundary conditions on B

$$(BV - B\nabla_X \phi - D_B \nabla B) \cdot \vec{n} = 0 \text{ on } \Gamma_l \cup \Gamma_r \quad \text{and} \quad \nabla B \cdot \vec{n} = 0 \text{ on } \Gamma_{in} \cup \Gamma_{out}.$$

It means that bacteria cannot cross the mucosa and flow through $\Gamma_{in} \cup \Gamma_{out}$ by transport.

Name	Meaning	Unit	Sigmoid distribution				Other value
			p_{max}	p_{min}	α_p	χ_p	
D_B	Bacteria diffusion	$\text{cm}^2 \text{d}^{-1}$	$5 \cdot 10^{-4}$	10^{-5}	12	$\frac{4}{5} L_x$	-
η	Stiffness of the function f	s		-			10
M_{ref}	Reference volume fraction of mucus for f	\emptyset		-			$\frac{4}{5}$
B_{max}	Maximal volume fraction of bacteria initial data for B_0	\emptyset		-			0.1
χ_B	Initial Gaussian function center for B_0	cm		-			$\frac{7}{10} L_x$
σ_B	Initial Gaussian function width for B_0	cm		-			25

TABLE 2. Biophysical constants of the extended model

We suppose that the volume fraction of bacteria is small compared to the amount of mucus or liquid, which leads us to assume the interface diffusion to be constant. We also suppose that the diffusion of bacteria grows with the amount of liquid. We set $P_{D_B} = (D_{B,max}, D_{B,min}, \alpha_B, \chi_B)$ and take

$$D_B(x, y) = \Sigma_{P_{D_B}}^-(x).$$

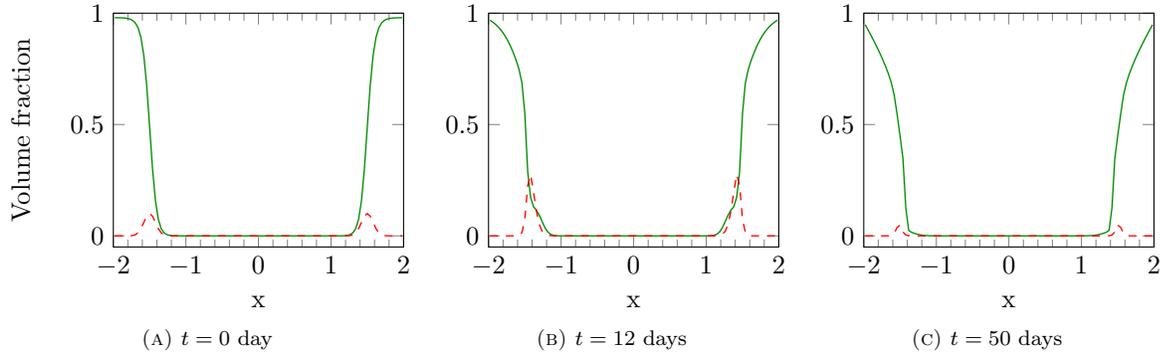


FIGURE 10. Cut view of mucus (green continuous line) and bacteria (red dashed line) volume fractions at different times at $y = -\frac{L_y}{2}$ for initial mucus profile $M_{0,s}$.

For the sake of simplicity, we assume that B_0 depends only on the horizontal coordinate with a profile defined by Gaussian functions centered on the interfaces liquid/mucus (see Fig. 10a)

$$B_0(x, y) = B_{max} \exp\left(-\frac{(x + \chi_B)^2}{2(L_x/\sigma_B)^2}\right) + B_{max} \exp\left(-\frac{(x - \chi_B)^2}{2(L_x/\sigma_B)^2}\right). \quad (21)$$

The parameters are collected in Table 2. Eq. (18) is treated like the conservation equation for M . The Poisson equation (20) is discretized with the VF4 scheme on pressure cells. The mean value in the right hand side, as well as the constraint on $\int \phi dX$, are approached by a suitable quadrature rule. We are led to solve an invertible linear system by introducing a Lagrange multiplier.

As in Section 5, we discuss the influence of the boundary data on Γ_{in} , depending whether or not u_{in} vanishes, and we check the behavior of the system when the mucus layer is perturbed. On Fig. 10b, the initial data for the mucus is a sigmoidal function $M_{0,s}$ and $u_{in} = 0$. We observe a neat concentration of the bacteria community at the abscissa $x = \pm 1.4$ where the mucus volume fraction is close to M_{ref} until $t = 12$ days. Then, the amount of bacteria starts to decrease and after 50 days, see Fig. 10c the volume fraction of bacteria is almost zero: the model is not able to conserve a bacterial population in the gut. Surprisingly enough, the behavior is different when we keep $u_{in} = 0$ and we change the initial data for the mucus to $M_{0,g}$, see Fig. 11a. A steady state, represented in Fig. 11b, is reached after 10 days: the profiles are indeed the same after 100 days, see Fig. 11c. In this state the bacterial community concentrates at the interface mucus/liquid, where the mucus volume fraction takes the value $M_{ref} = 0.4$. The mucus profile is slightly sharper than initially.

It is interesting to study the influence of the horizontal velocity at Γ_{in} . Instead of imposing $u_{in} = 0$ as above, we now set $u_{in} \neq 0$ as given by the iteration procedure at Sec. 5.1. Mucus and bacteria profiles at $t = 50$ and $t = 140$ days are displayed on Fig. 12 for the sigmoidal initial data $M_{0,s}$. Changing the boundary condition for u_{in} has completely changed the large time profiles: instead of a bacteria wash out, we observe an overgrowth of the bacterial population and a persistence in the domain. During the first 50 days, the total amount of bacteria is multiplied by eight and the maximal volume fraction of bacteria goes from 0.1 to 0.6, see Fig. 12a and 12b. Then the amount of bacteria decreases during a few days and stabilises with a maximal volume fraction around 0.5, see Fig. 12c. The mucus profile becomes also very specific: the luminal part is completely deformed around the bacterial aggregate. Some mucosal matter seems to be pushed laterally towards the lumen by the bacterial population, which occupies more and more volume. This fact can be related to a physiological observation: the soft layer of mucus has a greater volume than the hard layer due to the bacteria and the eukaryotic residuals that it contains. Note that, due to the high bacterial volume fraction at their distribution peak, the bacterial aggregate cannot be located where $M = M_{ref}$. The coupling with a bacterial population, which is furthermore

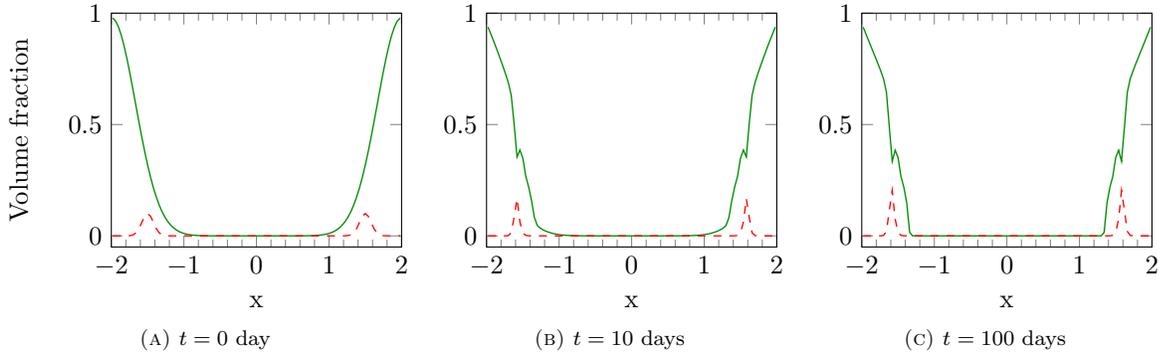


FIGURE 11. Cut view of mucus (green continuous line) and bacteria (red dashed line) volume fractions at different times at $y = -\frac{L_y}{2}$ for initial mucus profile $M_{0,g}$.

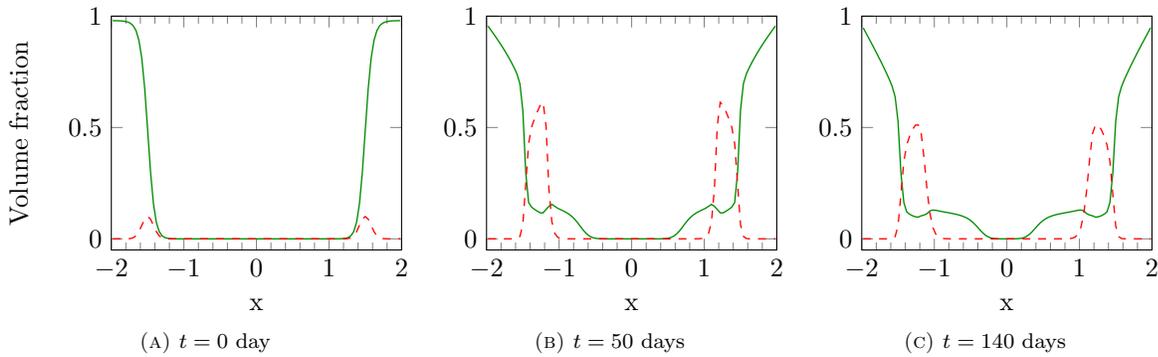


FIGURE 12. Cut view of mucus (green continuous line) and bacteria (red dashed line) volume fractions at different times at $y = -\frac{L_y}{2}$ for $M_{0,s}$ and $u_{in} \neq 0$ in the iterative procedure of Sec. 5.1.

driven by chemotactic mechanisms, makes the model more sensitive, in particular with respect to uncertainties on the horizontal velocities, and its behavior is more intricate. This preliminary attempt provides interesting and relevant avenues for reflection, that will be further investigated elsewhere.

We finally investigate the recovery of the mucus layer when the initial condition is perturbed and the bacterial population is present. We take the same protocol as in Section 5. We start with $M = M_{0,p}$ at $t = 0$ and take the result of the iterative process as boundary condition on the boundary. The bacteria population initial distribution is sigmoidal until $y = -4$ and uniformly zero for $-4 \geq y \geq -L_y$. Several snapshots of the simulation are displayed in Fig. 13. We can see that the mucus layer reconstruction dynamics is visually unchanged: a mucus layer is recovered after a few days through the overlapping of the disrupted zone by a uphill tongue of mucus. We can see the complex interaction of the bacterial population with the mucus layer near the tongue of mucus. At $t = 2$ and $t = 3$ days, we can observe that some bacteria are transported uphill and get into the interstitial space between the mucus tongue and the mucus layer near the mucosa. At $t = 50$, we observe some mucus in the lumen of the gut, reflecting the deformation of the mucus front by the bacterial population.

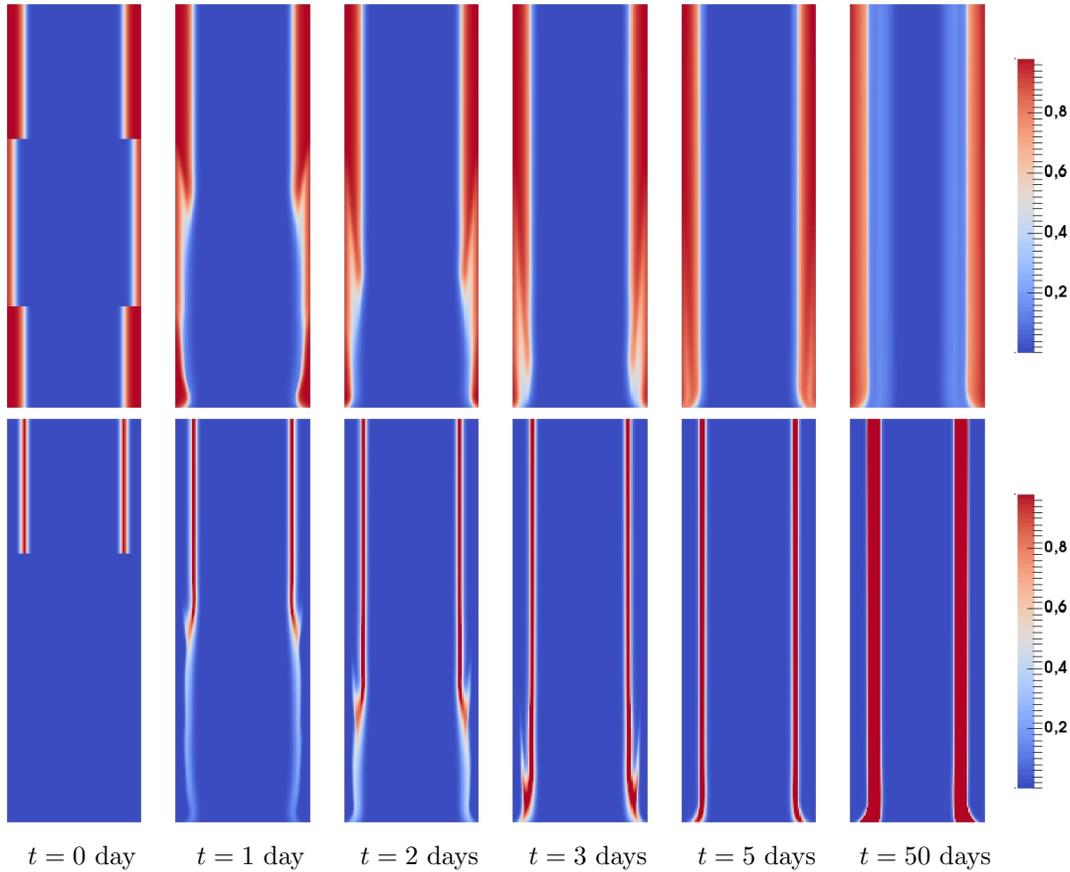


FIGURE 13. Evolution in time of the disrupted mucus layer together with the chemotactic bacterial population. We present the mucus (upper row) and bacteria (lower row) volume fraction maps at different times in order to illustrate the reconstitution of the steady-state mucus layer when a chemotactic bacterial population is present.

8. CONCLUSION

We have proposed a model, inspired from mixture theory, which is able to describe the formation of a stable layer of mucus in the gut. The modelling relies on a short list of simple biological mechanisms — mucus production, liquid pumping, viscosity discrepancies between liquid and mucus, relevant inflow. Interaction with populations of bacteria can be incorporated in the equations, and the model reproduces the mucus layer flattening due to the penetration of the bacteria into the luminal part of the mucus layer. Such a model can take into account different biological knowledges to contribute to a better understanding of the microbial population dynamics and the host-microbiota interactions, especially through the mucus layer. This set of PDE can be used to investigate several pathological disorders of the mucus. For instance, by modifying the shape of the viscosity function $M \mapsto \mu(M)$ we can describe rheological disorders due to mucin composition or conformation. Through the functions f_M and f_L , we can account for mucus layer disruptions that arise in several bowel diseases, such as the inflammatory bowel disease (IBD).

This work remains a first attempt and it is worth pointing a few relevant improvements of the model that will deserve to be further investigated. Curvature effects should be taken into account by considering a cylindrical geometry. The boundary conditions, which are crucial for determining the shape of the mucus layer, should

take into account the fluid/structure interactions that occur during peristaltism: the periodic contraction of the mucosa produces longitudinal traveling waves that ease the intestinal transit. Such a difficulty is common in the modeling of biological flows [1]. Accounting for the bacterial gas production is also an issue since it can influence the intestinal fluids flows. We are using a model based on mixture theory, which involves a closure relation describing diffusion effects. The definition of the diffusion coefficients is a crucial modeling issue. It enters both in the equation in the domain and in the boundary conditions for the constituents volume fractions. It would be natural to work with coefficients that depend on the mucus volume fraction, thus inducing further non linearities in the equations. Here, we have adopted a quite phenomenological viewpoint by imposing a specific space-dependent profile to the coefficients D_M, D_L . The formula should be understood as a rough way to describe the complex interaction of the mucus layer with the gut wall. The knowledge of these interactions is not well-advanced but it is clear from the observation that they are mechanisms able to keep the mucus attached to the wall. For instance, it would be interesting to take into account more precisely the impact of the microscopic nature of this interaction on the diffusion distribution through suitable homogenization methods.

The model for the bulk velocity could also incorporate additional viscosity term, as described in Remark 2.1, which would equally impact, and possibly improve, the definition of the boundary conditions. In order to describe more accurately the mucus stratification, the definition of the viscosity function should be improved, taking into account the different rheological properties of the mucus layers. Another relevant modeling option would be to set up a model with momentum balance equations for the velocities u_M, u_L of the constituents.

Finally, we have adopted a quite naive and phenomenological description of the chemotactic mechanisms that bacteria are subjected to; future developments should try to reflect more closely the biological mechanisms.

The work presented in this paper is the result of a fruitful collaboration that took place during the CEMRACS 2015. We warmly thank the organizers of the 2015 edition of the CEMRACS: Emmanuel Frénod (UBS Vannes), Emmanuel Maitre (U. Grenoble), Antoine Rousseau (Inria Montpellier), Stéphanie Salmon (URCA Reims), and Marcela Szopos (U. Strasbourg). We also thank the referees for useful remarks and comments regarding the manuscript.

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